



## ■ Water Treatment of Central Air-conditioning Cooling System

## ■ Agenda

- Purpose of Water Treatment
- Difficulties of balancing among Corrosion, Scaling and Algae Control
- Treatment Theory (LSI)
- Successful Factor of Water Treatment
- Real-Time Water Treatment Automation System
- Q & A

## Purpose of Water Treatment

## ■ Purpose Of Water Treatment

*“Water Treatment Plays a vital role in **protecting** the MEP asset as well as to increase **system efficiency**”*

- *Prolong major equipment life-cycle by preventing **breakdown** or **premature failure** — equipment such as Cooling Tower, Chillers & Boiler*
- *Reduce any business risk/equipment **downtime**.*
- *Increase plant **efficiency**.*
- *Reduce environmental impact by **optimizing water, energy and waste output**.*
- *Reduce total cost of operation and repairs*

*Water Treatment is an important part of your preventive maintenance in up keeping the MEP Assets.*

# ■ Purpose of Water Treatment

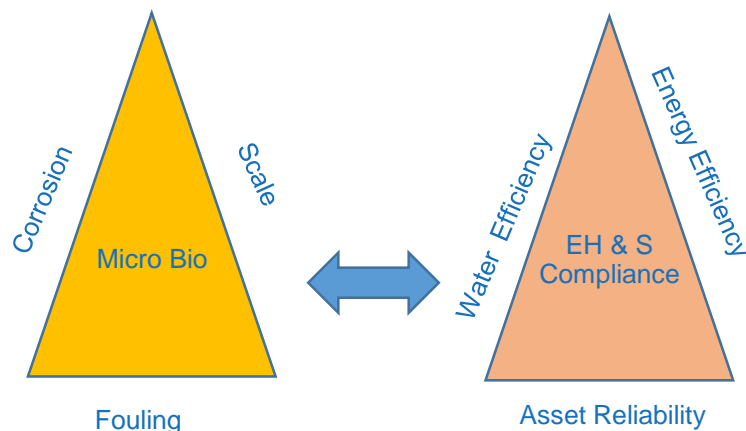
*Water Treatment Program is to mainly prevent,*

- *Corrosion*
- *Scale*
- *Micro Bacteria*
- *Fouling*

*By this means,*

*Water Treatment Program enhance,*

- *Asset Reliability*
- *Water & Energy Efficiency*
- *By eliminating wastages*
- *EH & S Compliance*



## Difficulties of Balancing among Corrosion, Scaling & Algae Control

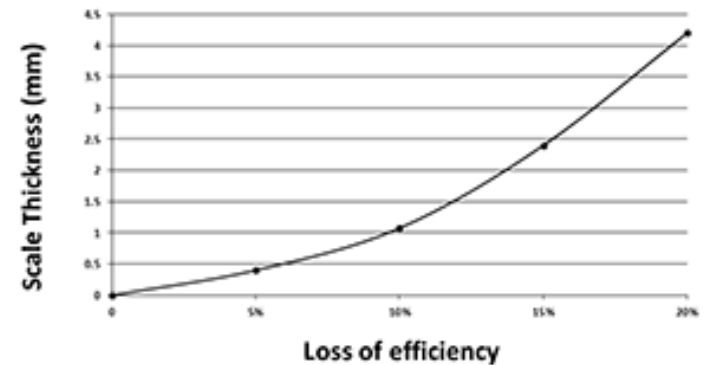
# ■ Difficulties of Balancing Corrosion, Scale and Algae

## • Impact of Scale

- Every formation of the scales will reduce the efficiency of heat transfer thus is an increase of cost of operation.
- The impact of scales on cost increment is exponential.



## Scale Inflates Operating Costs



EQUIPMENT	KW/TON	LOAD FACTOR	OPERATING HOURS	KWH/RATE	ENERGY COST
500 TON CHILLER	x .65	x 100%	x 6,570	\$ .09	= \$192,173

DEPOSIT THICKNESS (Inches)	% EFFICIENCY LOSS	INCREASED ENERGY COST
0.01	9%	\$17,296
0.02	18%	\$34,609
0.03	27%	\$51,887
0.04	36%	\$69,182
0.05	45%	\$86,478

Just 1/32 of an inch of scale can add nearly \$52,000 to the cost of operating a 500-ton chiller!

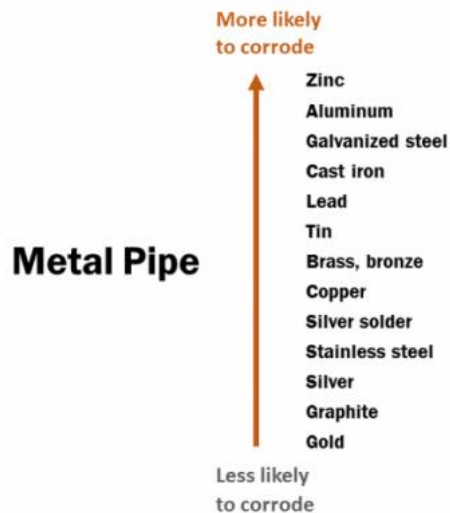
ENERGY SAVINGS 0.03" DEPOSIT	CHEMICAL CLEANING COST (EST.)	ANNUAL NET SAVINGS
\$51,887	\$900.00	= \$50,987



# ■ Difficulties of Balancing Corrosion, Scale and Algae

- Impact of Corrosion

- Corrosion of the tube lead to inefficiency fluid flow and heat transfer thus increase in the cost of operation.
- The impact of corrosion is irreversible. The only remedy to serious corrosion is only replacement of the part.

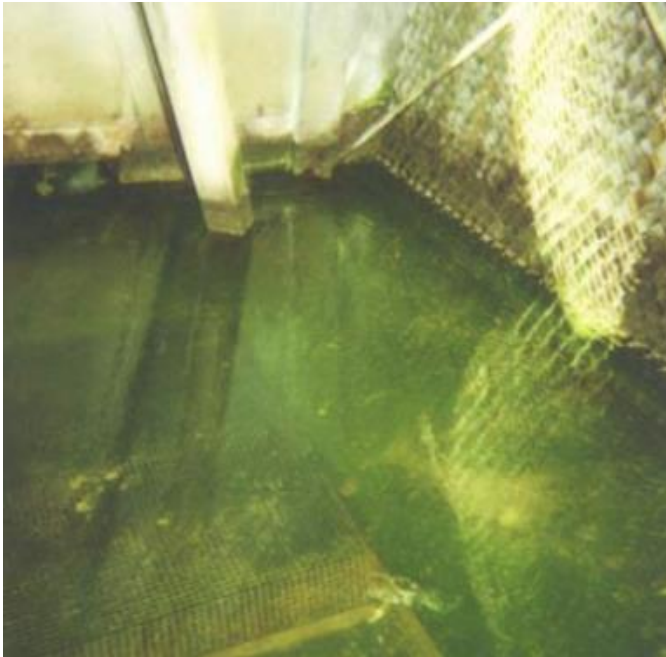




# ■ Difficulties of Balancing Corrosion, Scale and Algae

- Impact of Algae

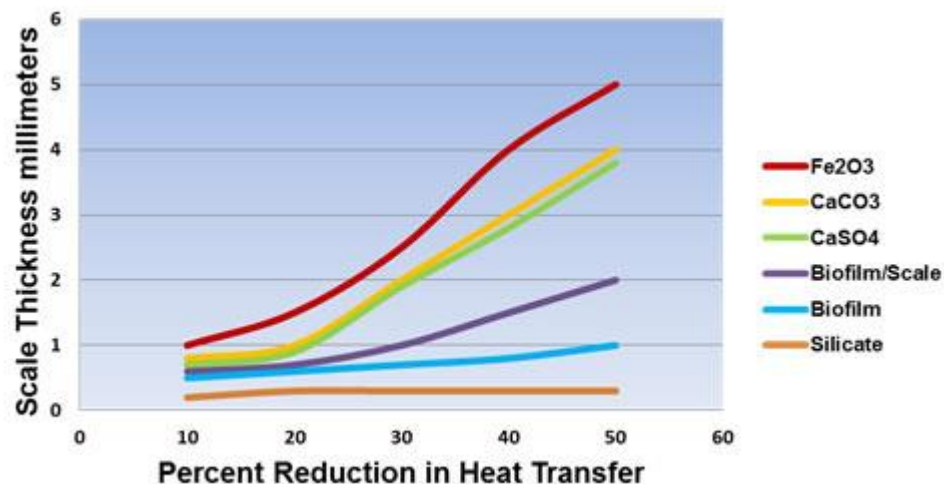
- Increases nutrient in cooling water
- Increase mechanical cleaning
- Increase bacteria like SPC, Legionella
- Reduces water heat exchange



# ■ Difficulties of Balancing Corrosion, Scale and Algae

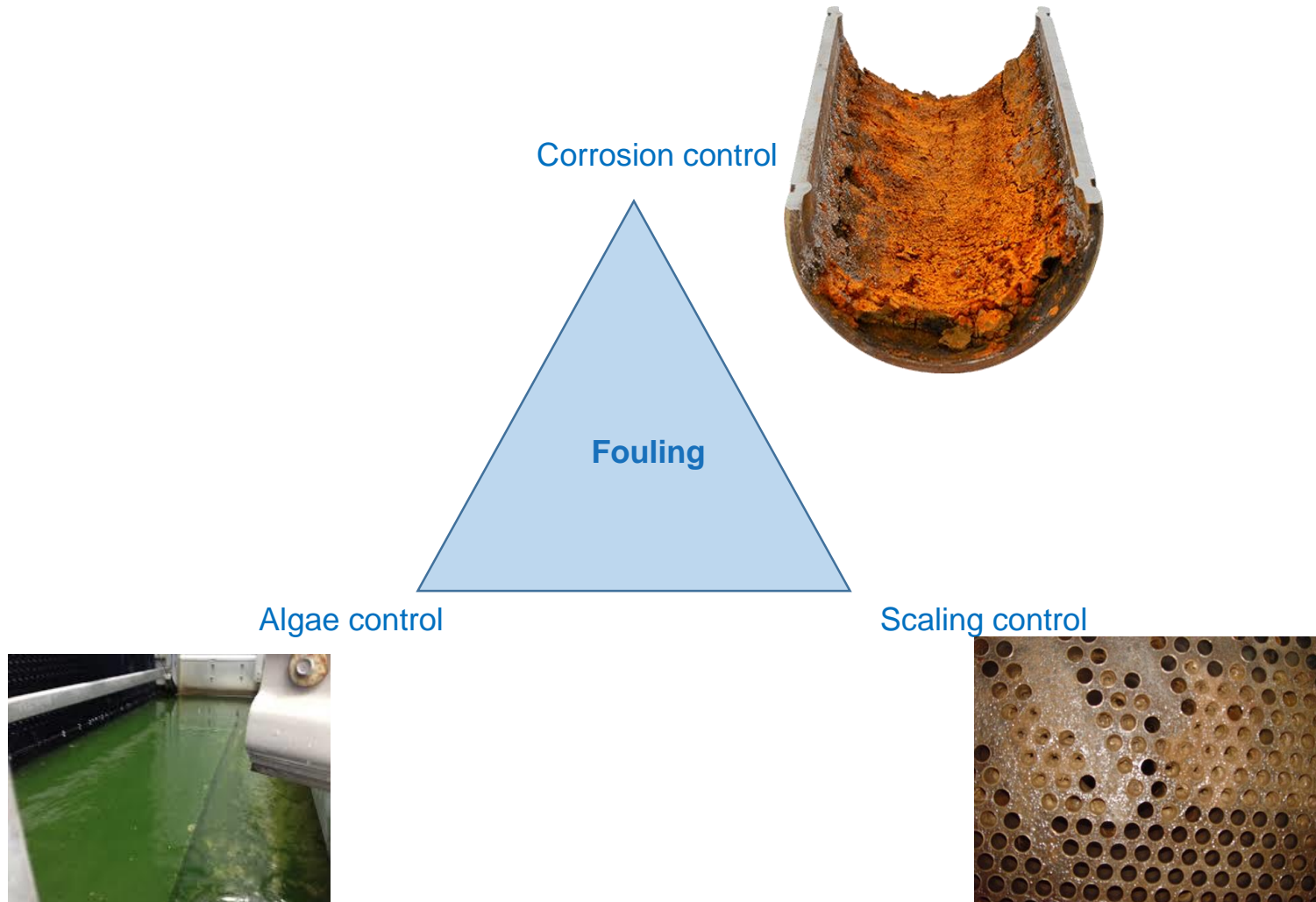
## • Impact of Bio-Film

- Bio-Film creates layer of organic insulation that reduce heat transfer efficiency.
- The impact of bio-film on heat efficiency reduction is serious than most of the scale.
- Bio-Film also increase the risk of Legionella outbreak.



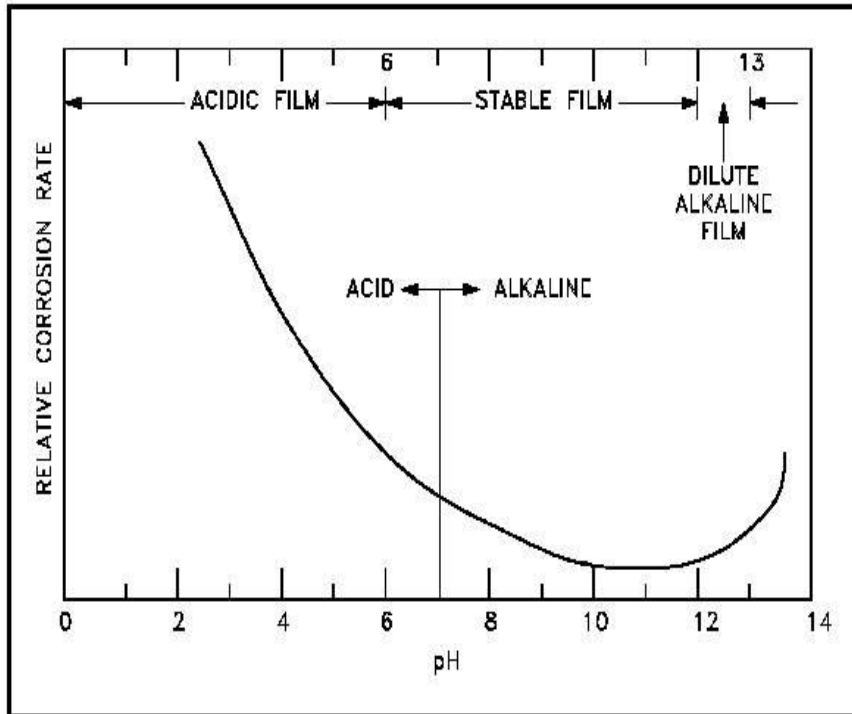
# ■ Difficulties of Balancing Corrosion, Scale and Algae

## Water Balancing ?

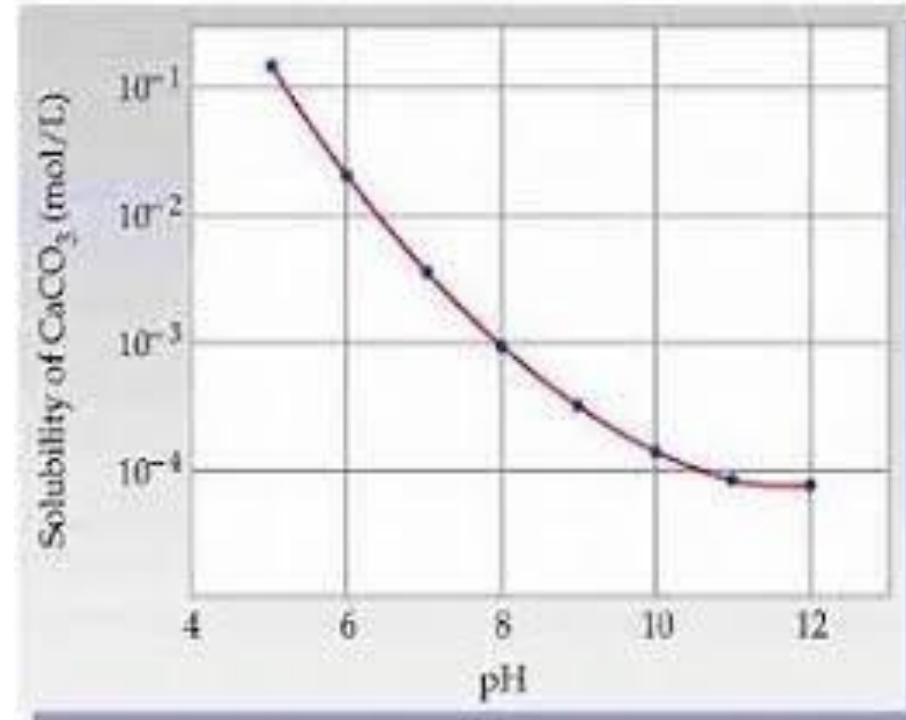


# ■ Difficulties of Balancing Corrosion, Scale and Algae

## Water Balancing ?



High pH , low corrosion rate



High pH , High Scaling

## ■ Difficulties of Balancing Corrosion, Scale and Algae

What Influence all the above?

- Conductivity
- pH
- Alkalinity
- Hardness
- System Design & Operation (Temp, hrs , metallurgy)

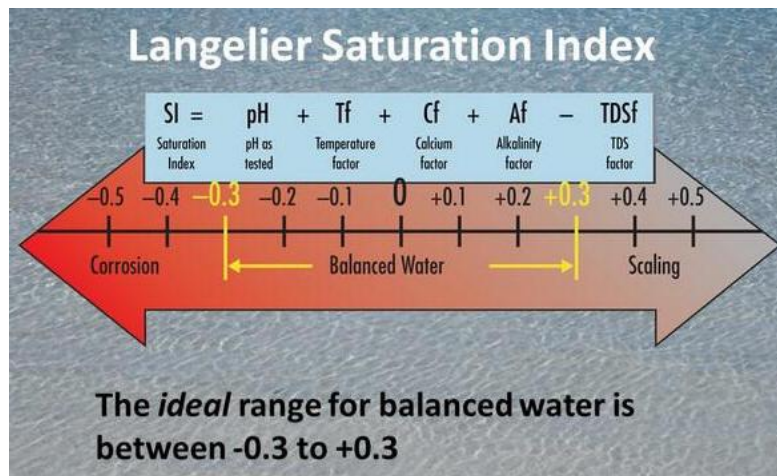
## Treatment Theory (LSI)



# ■ Treatment Theory (LSI)

## • What is LSI ?

- Langelier Saturation Index (LSI)
- Theoretical concept of saturation water
- Provides indicator of degree of saturation of water with respect to Calcium Carbonate.
- It base on 10 logarithm of Calcite Saturation Level
- Determine by pH equilibrium in the water



$$LSI = pH - pH_s$$

•Where:

- pH is the measured water pH
- $pH_s$  is the pH at saturation in calcite or calcium carbonate and is defined as:

$$pH_s = (9.3 + A + B) - (C + D)$$

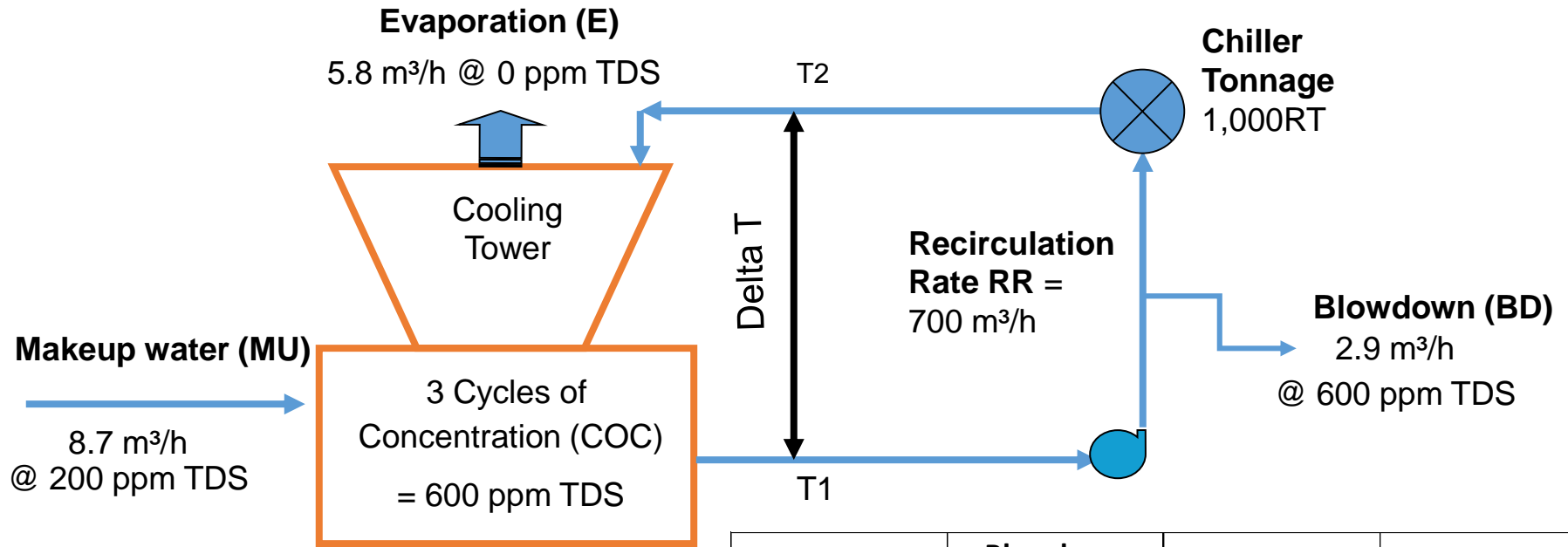
•Where:

- $A = (\log_{10} [TDS] - 1) / 10$
- $B = -13.12 \times \log_{10} (^\circ C + 273) + 34.55$
- $C = \log_{10} [Ca^{2+} \text{ as } CaCO_3] - 0.4$
- $D = \log_{10} [\text{alkalinity as } CaCO_3]$

- If LSI is negative: No potential to scale, the water will dissolve  $CaCO_3$
- If LSI is positive: Scale can form and  $CaCO_3$  precipitation may occur
- If LSI is close to zero: Borderline scale potential



# ■ Treatment Theory (LSI)



## Mass Balance

$$MU = E + BD$$

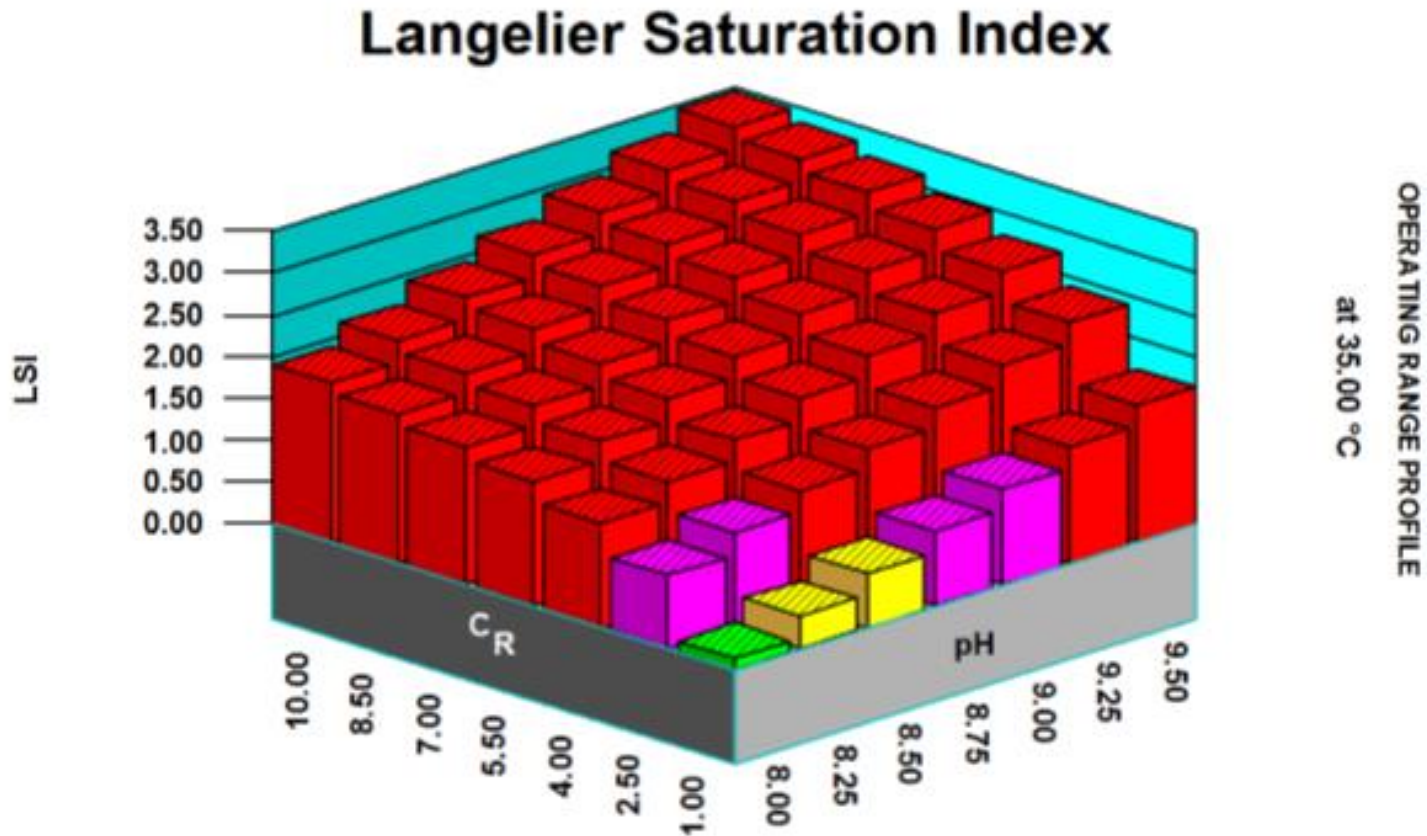
$$CoC = MU/BD$$

Or,

$$= TDS_{BD} / TDS_{MU}$$

Cycles of Concentration	Blowdown Water m <sup>3</sup> /h	Makeup Water m <sup>3</sup> /h	Evaporation m <sup>3</sup> /h
3	2.9	8.7	5.8
4	1.9	7.7	5.8
5	1.4	7.2	5.8
6	1.2	6.9	5.8
7	1.0	6.8	5.8
8	0.8	6.6	5.8
9	0.7	6.5	5.8
10	0.6	6.4	5.8

## ■ Treatment Theory (LSI)

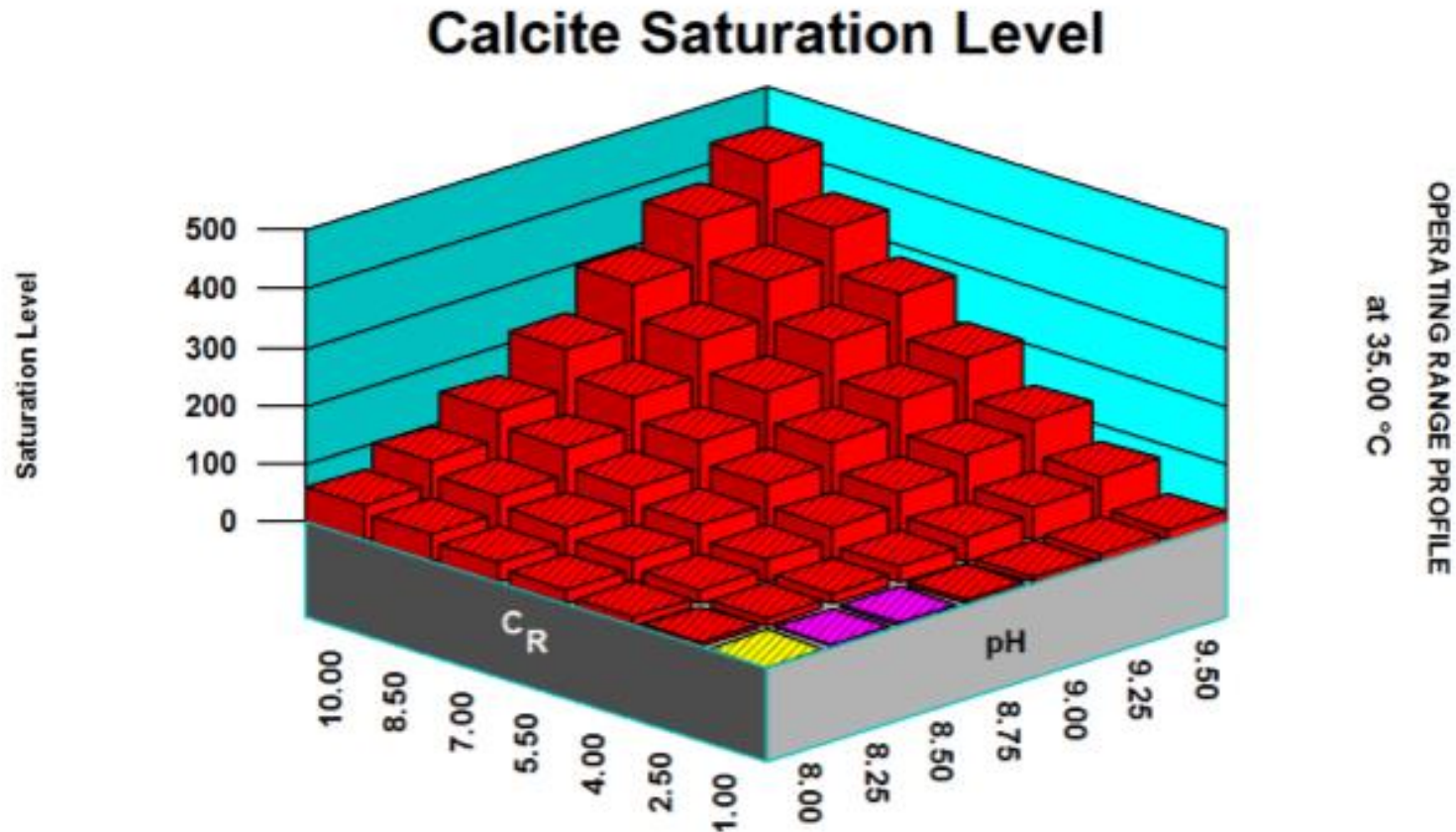


**\*\* It shown that, pH higher 8, cycle higher 4, at 35 deg. C of cooling tower water, very high tendency to scale\*\***

Langelier Saturation Index : Most common scaling predicting index

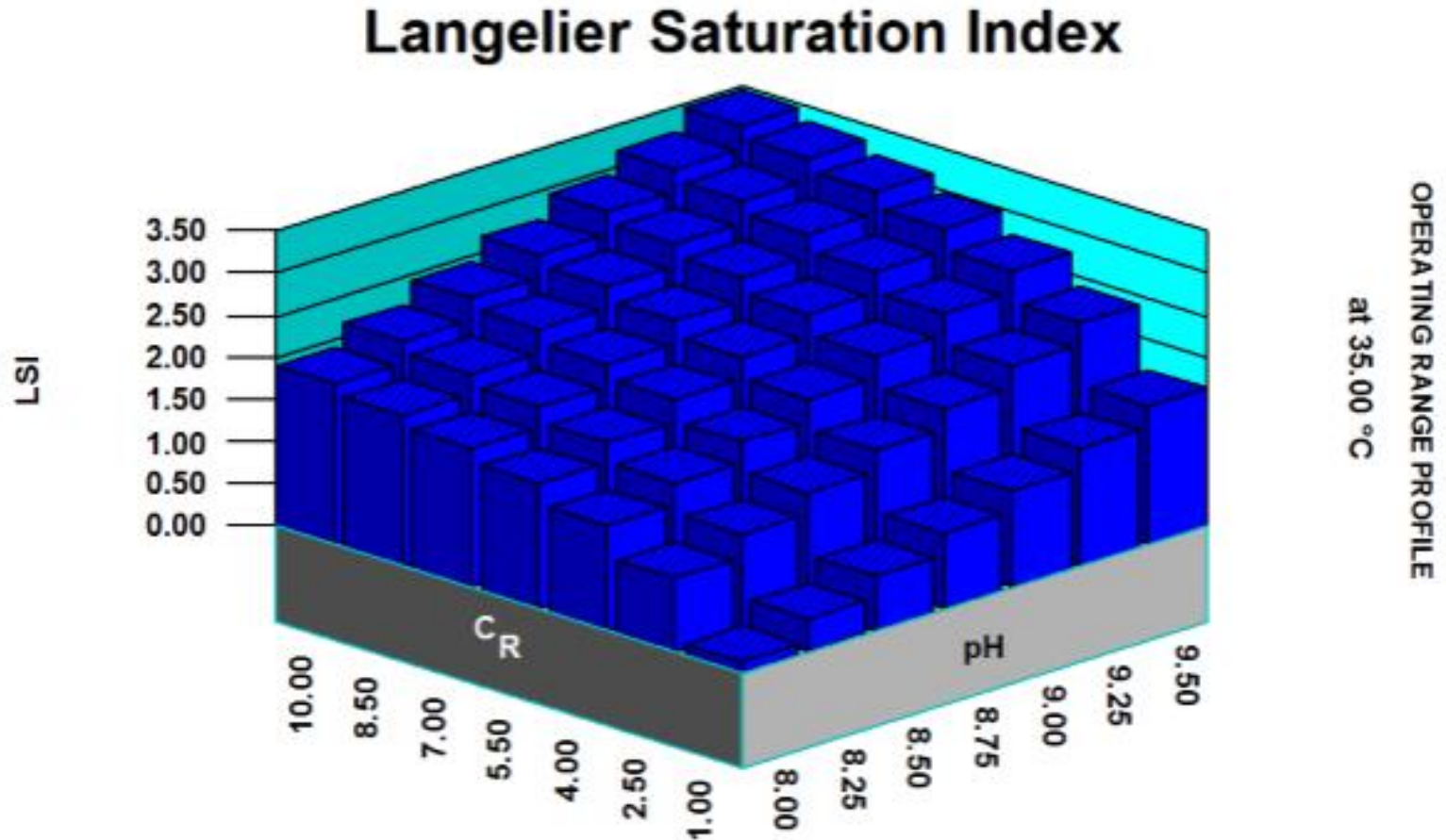
## ■ Treatment Theory (LSI)

Also, the below is the calcium carbonate scaling tendency chart under different pH and CR (cycle of recirculation).



## ■ Treatment Theory (LSI)

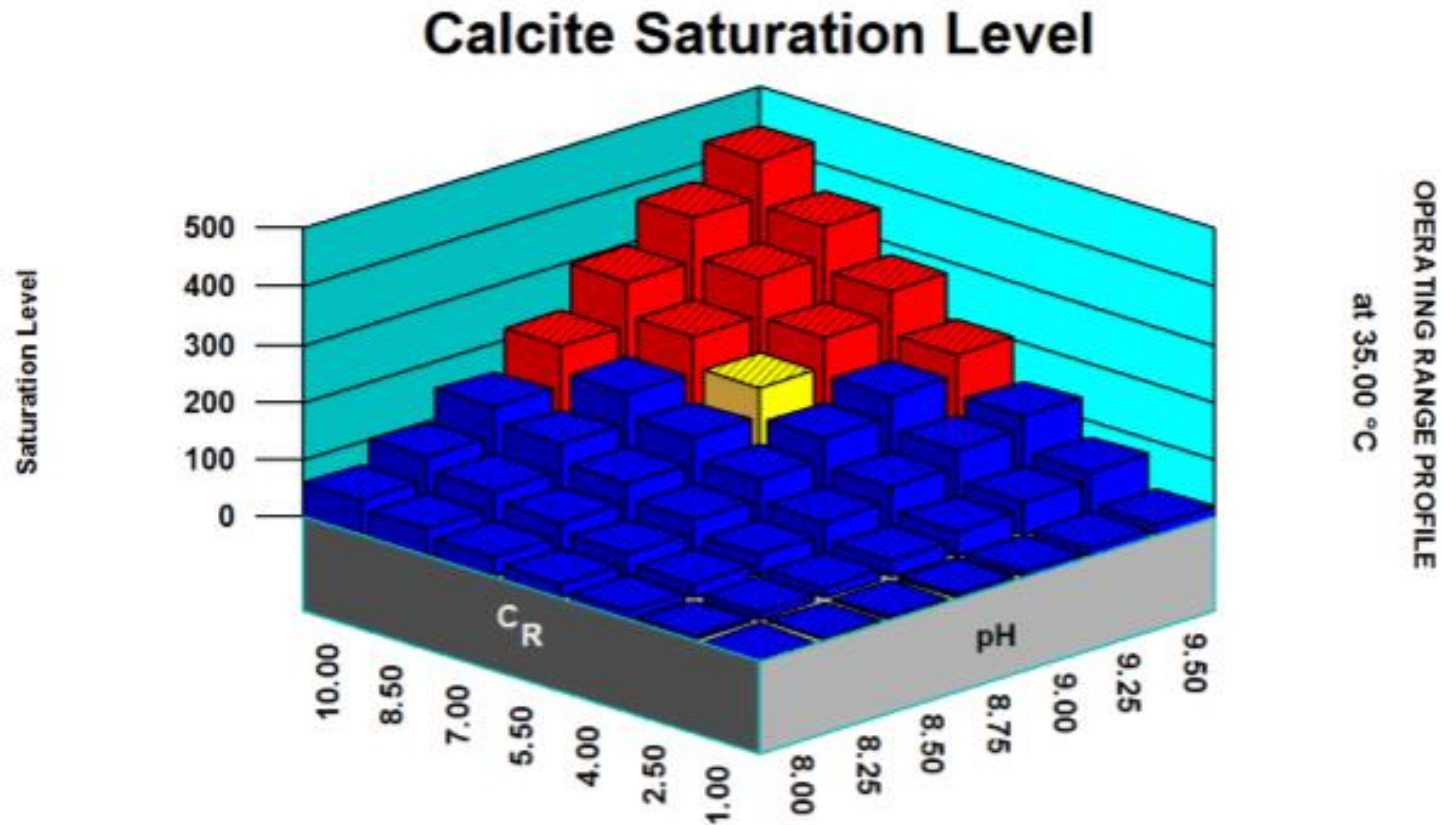
- After that, we dose 100ppm Chem-aqua 31155, and provide pH control between +/- 0.1 of 8.2.





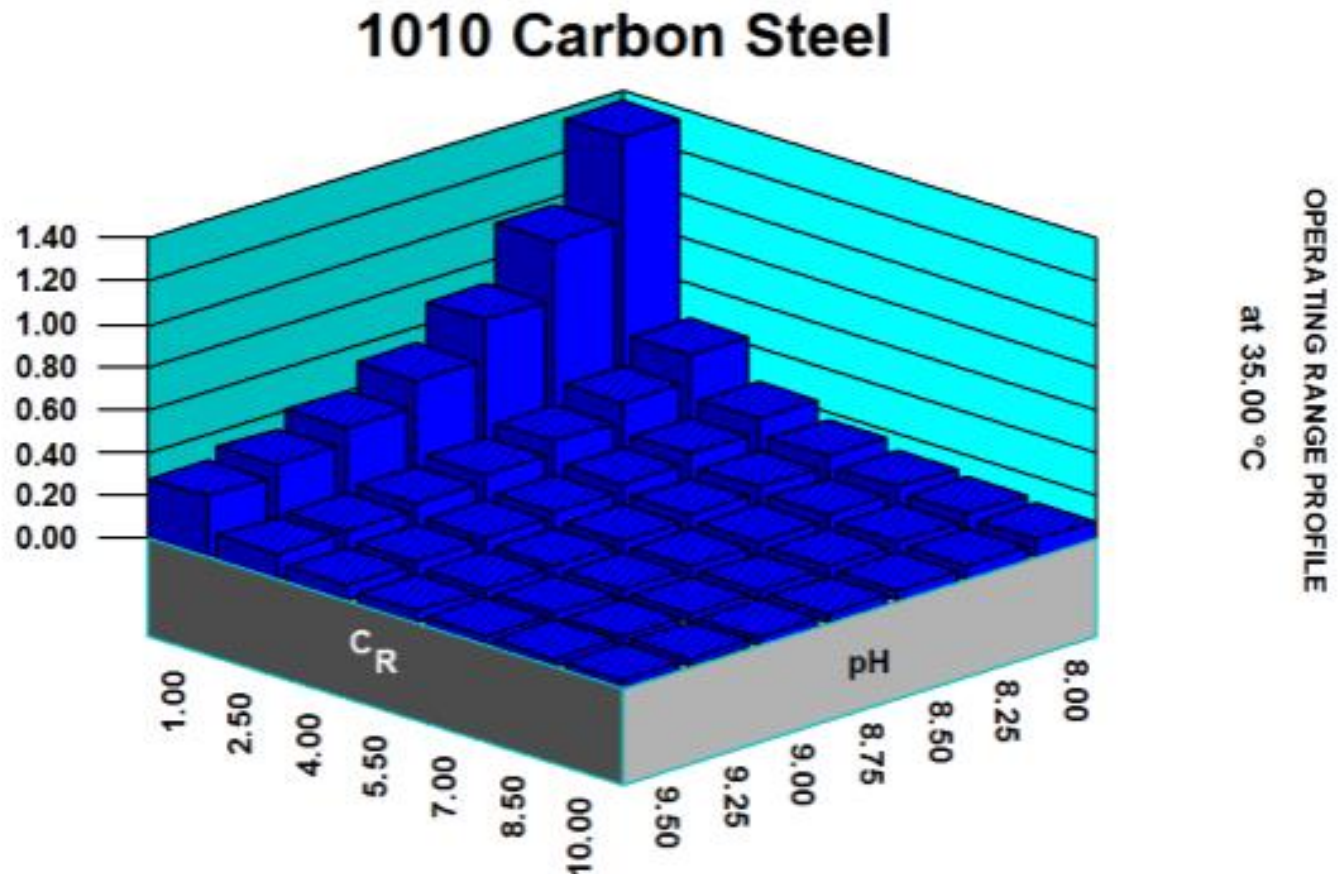
## ■ Treatment Theory (LSI)

And, the corrosion rate of carbon steel and calcium carbonate scaling tendency estimated scenario as below:



<< For pH 8.2: +/- 0.1 and Cycle kept at 8, scaling tendency is very low >>

## ■ Treatment Theory (LSI)



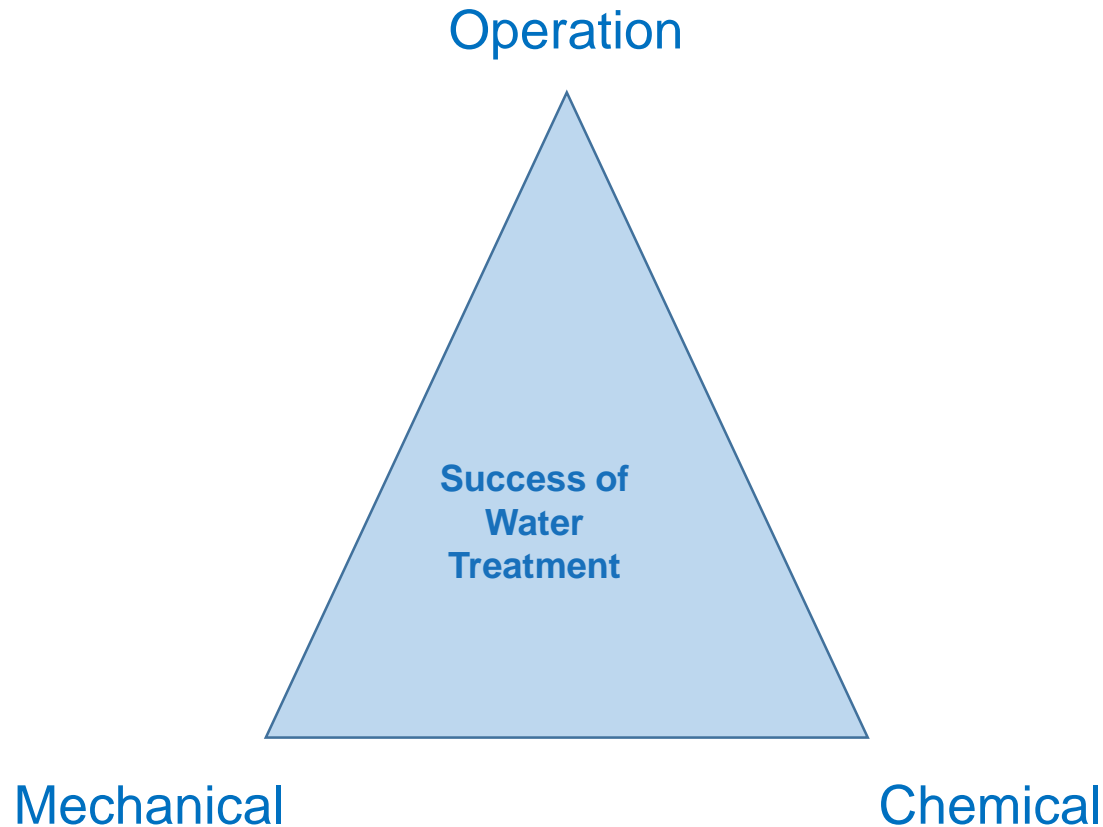
<< with dose CA31155, estimated carbon steel corrosion rate is only 0.1 or 0.2 MPY >>

## Successful Factor of Water Treatment



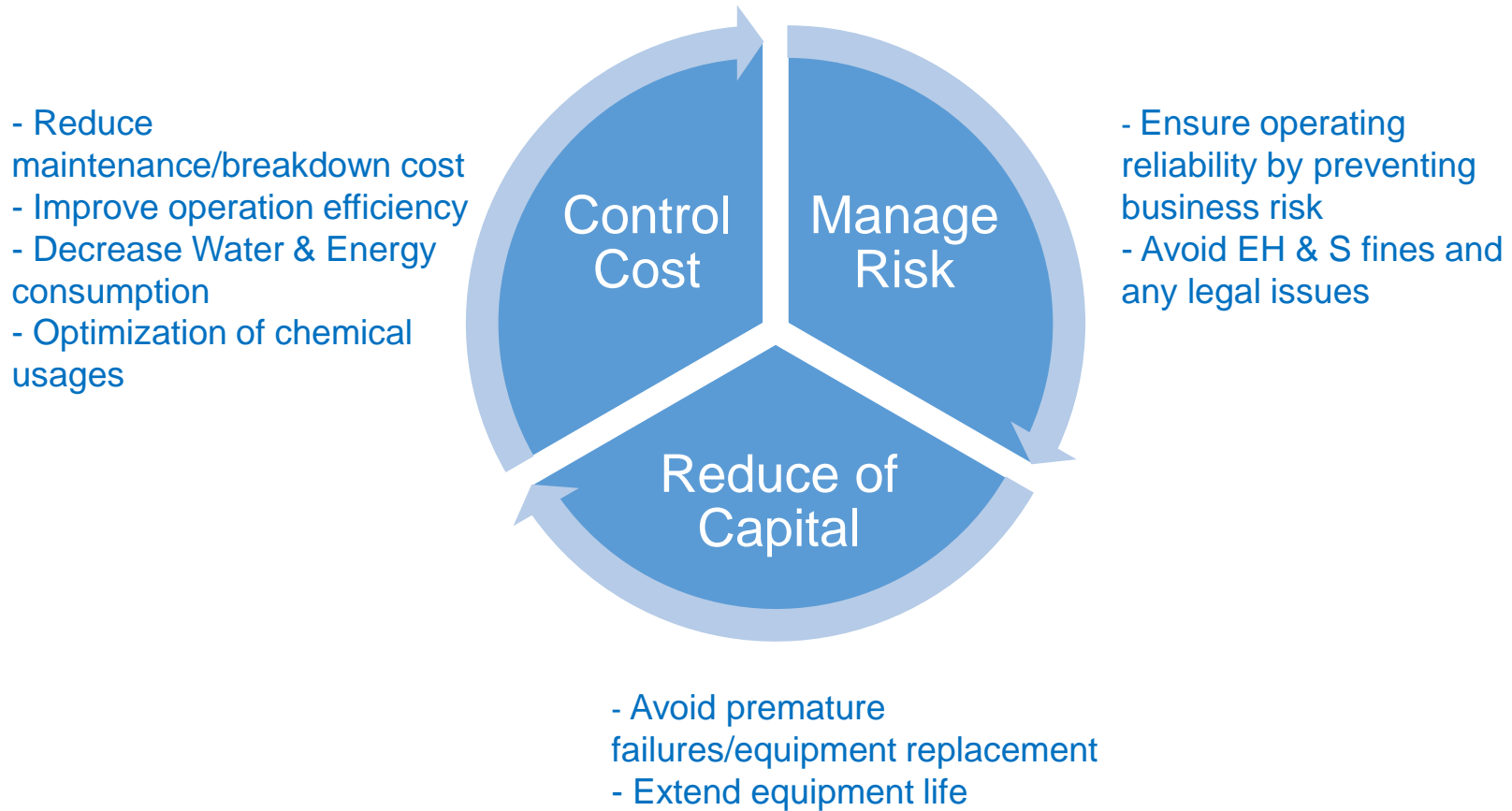
## ■ Successful Factor of Water Treatment - Summary

*“MOC” Approached*



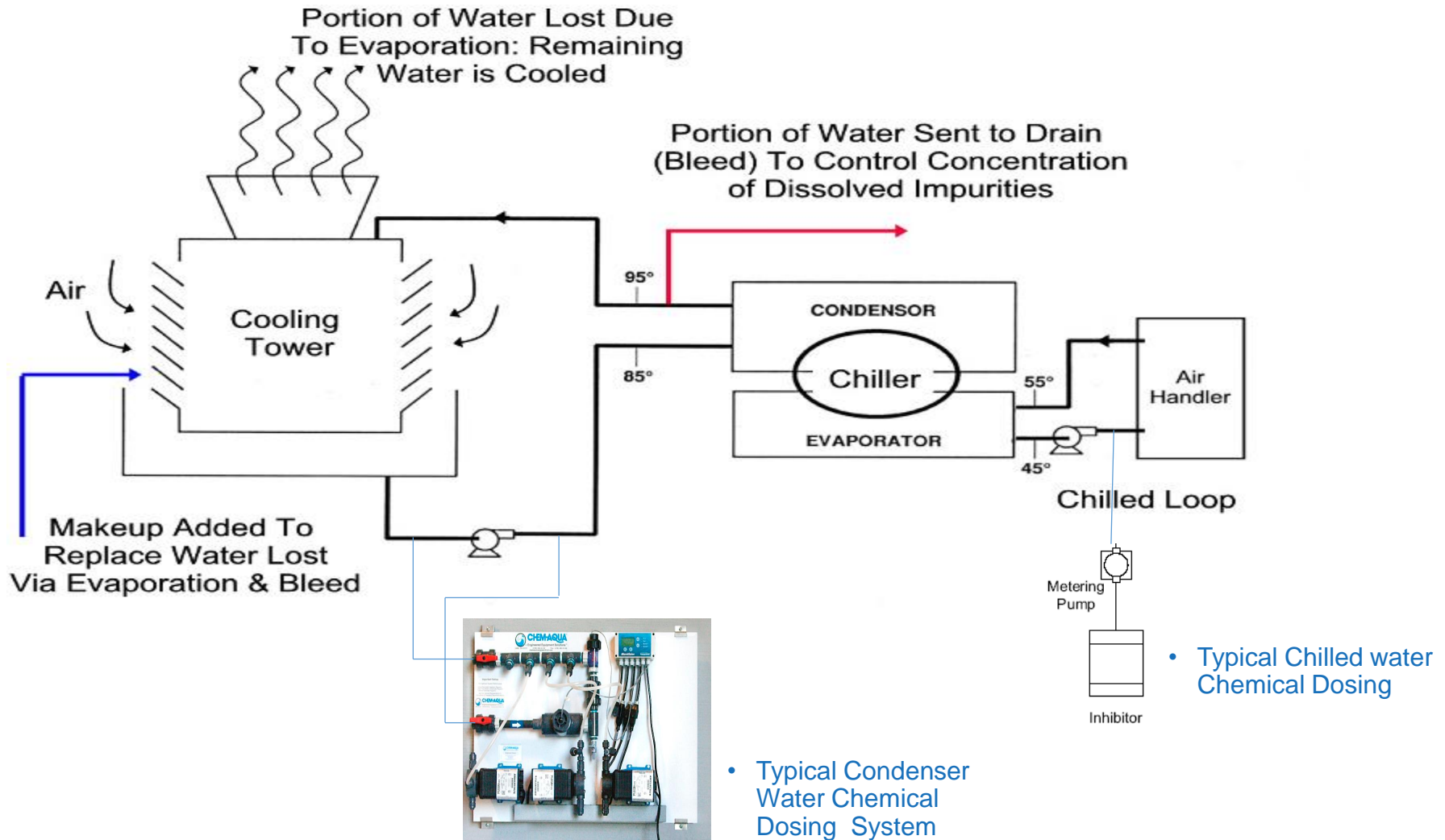
## ■ Successful Factor of Water Treatment - Summary

### *Effective Water Treatment*



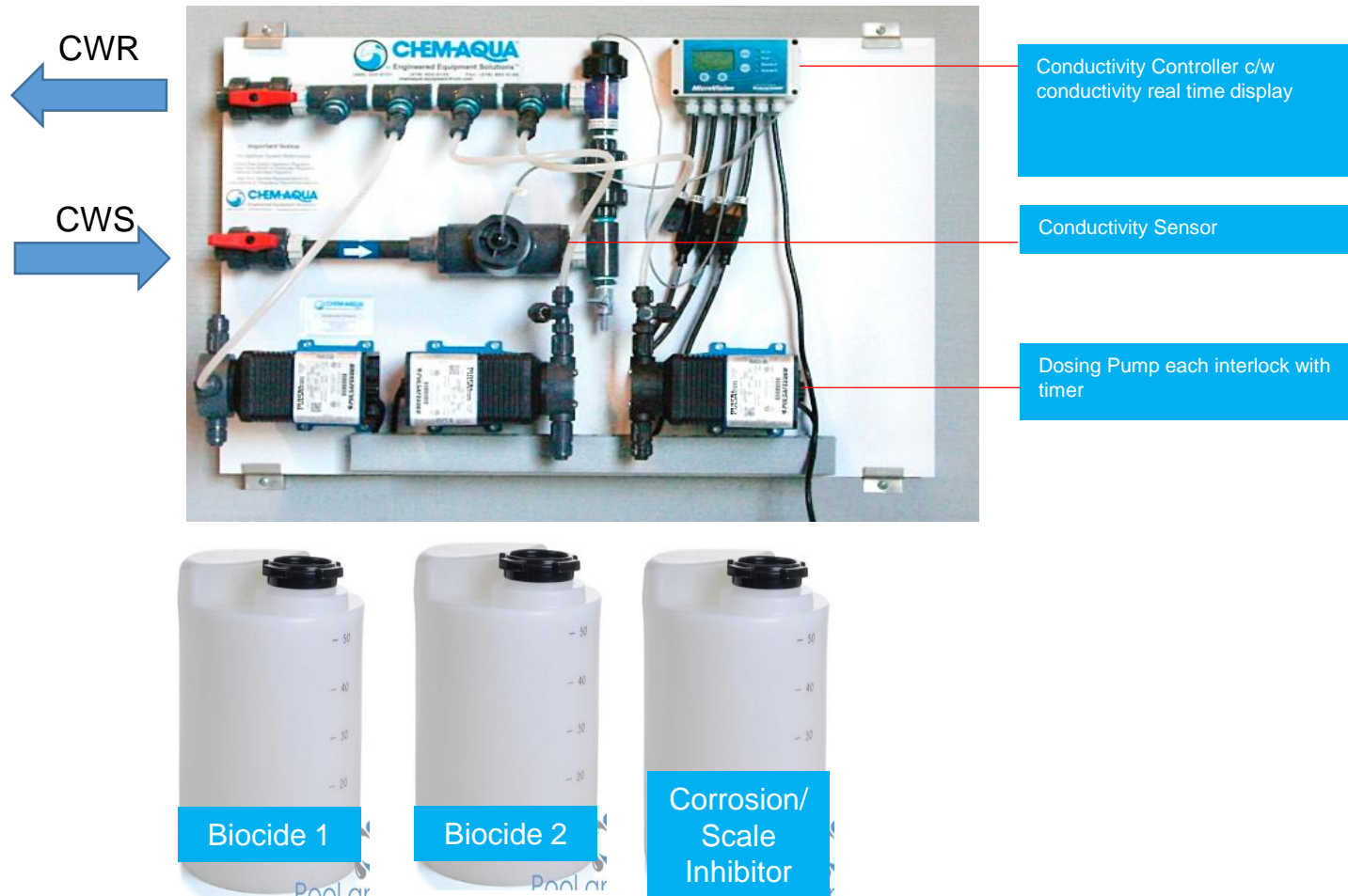
# Real-time Water Treatment Automation System

# Real-time Water Treatment Automation System



# Real- time Water Treatment Automation System

## Conventional Water Treatment Automation System



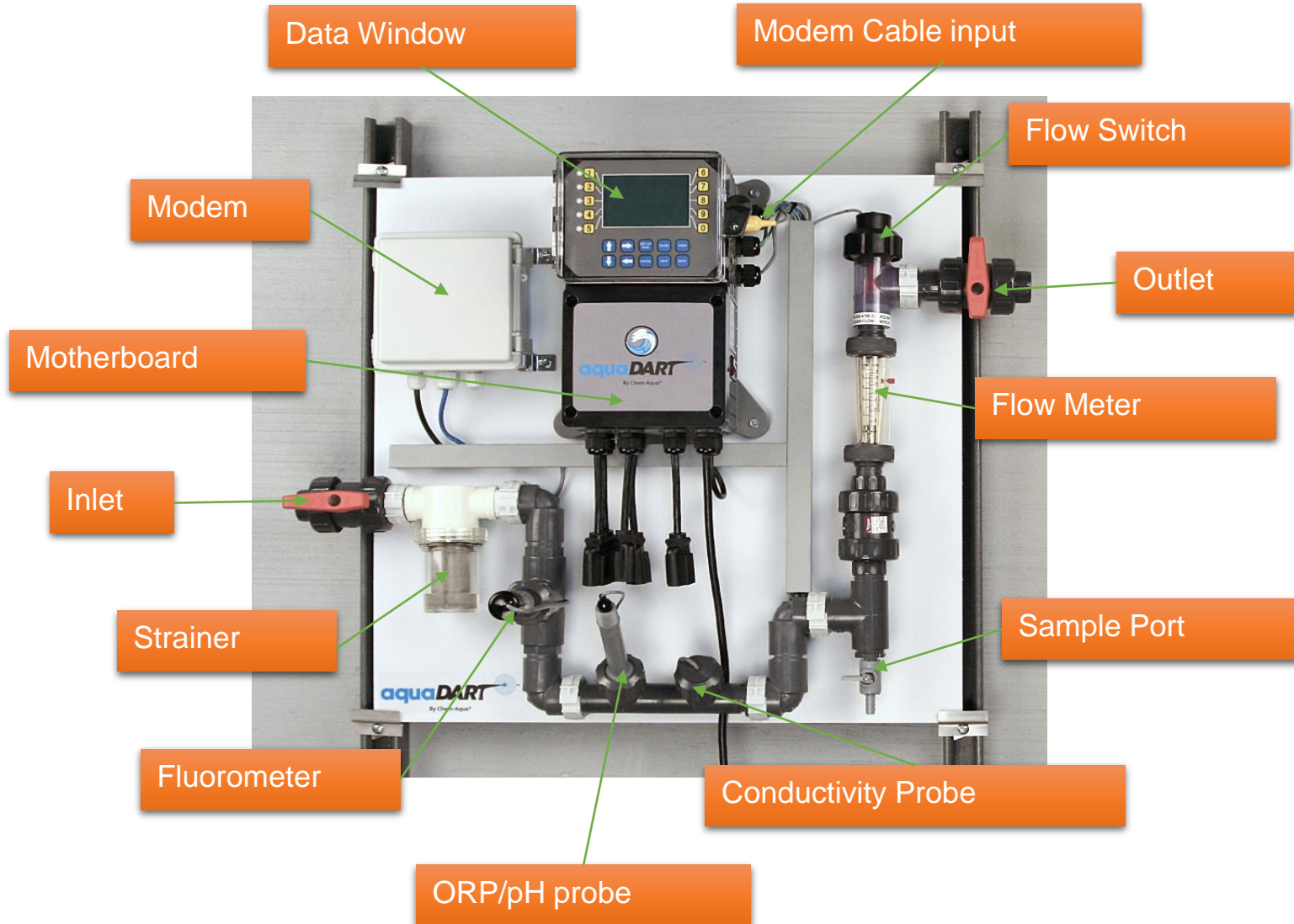
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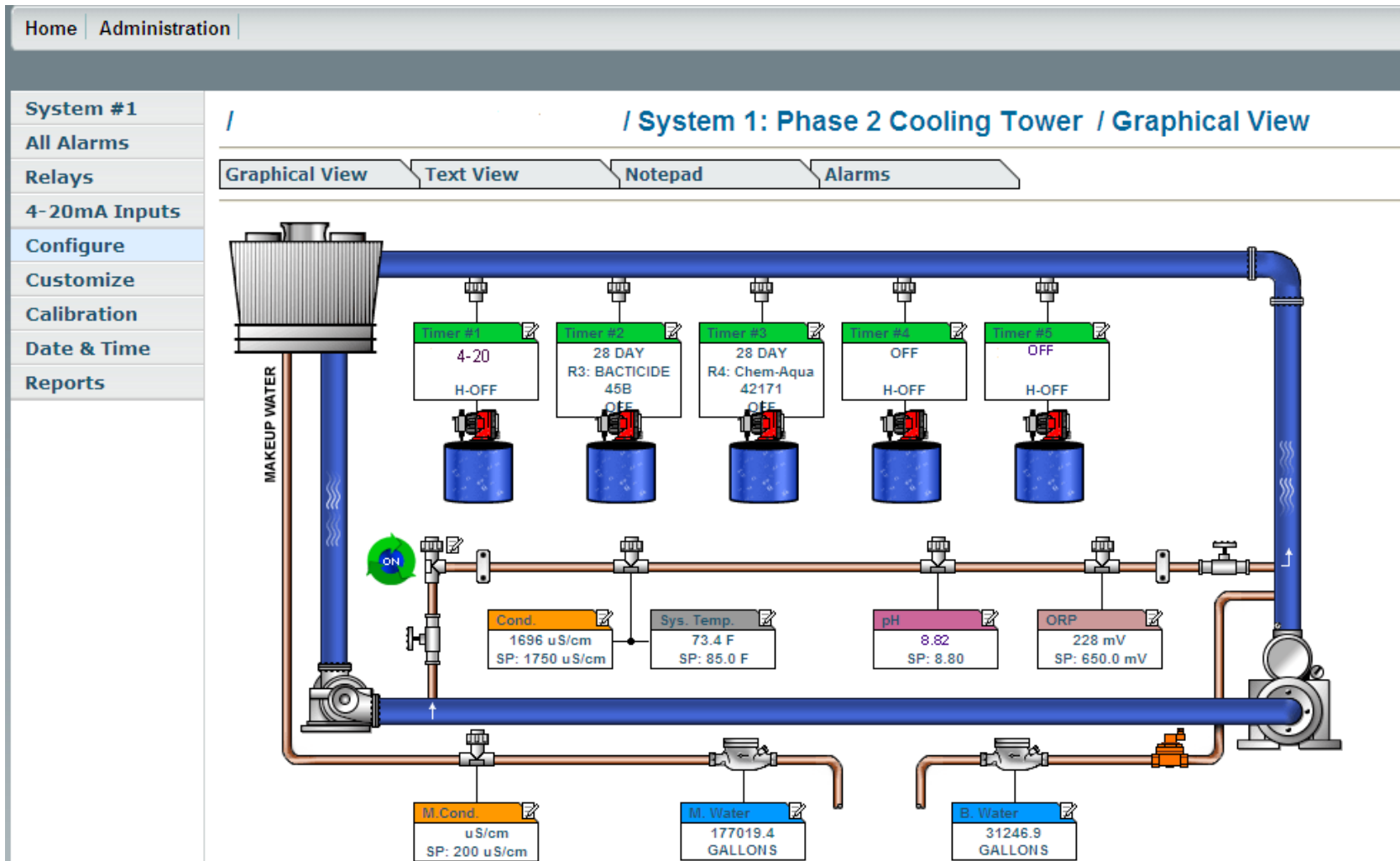
# ■ Real- time Water Treatment Automation System

## Web Base Communications



# Real-time Water Treatment Automation System

## Web Base Interface



# Real- time Water Treatment Automation System

## Web Base Interface

[Home](#) | [Administration](#)

[System #1](#)  
[All Alarms](#)  
[Relays](#)  
[4-20mA Inputs](#)  
[Configure](#)  
[Customize](#)  
[Calibration](#)  
[Date & Time](#)  
[Reports](#)

/

/ System 1: Phase 2 Cooling Tower / Text View

Graphical View

Text View

Notepad

Alarms

Sensors			
Name	Reading	UOM	Setpoint
Conductivity	1747	uS/cm	1750
System Temp	71.0	F	85.0
pH	4.98		8.80
ORP	228	mV	650.0
M. Conductivity		uS/cm	200
M. Temp	0.1	F	85.0
Flow	ON		

Timers			
Name	Type	Relay	Status
Timer #1	4-20	R1: Chem-Aqua 33155	H-OFF
Timer #2	28 DAY	R3: BACTICIDE 45B	OFF
Timer #3	28 DAY	R4: Chem-Aqua 42171	OFF
Timer #4	OFF		H-OFF
Timer #5			H-OFF

Digital Inputs		
Name	Status	Alarm Notification
D1	OFF	OFF
D2	OFF	OFF
D3	OFF	OFF
D4	OFF	OFF
D5	OFF	OFF

Water Meters		
Name	Reading	UOM
Water Meter #1	177035.6	GALLONS
Water Meter #2	31247.6	GALLONS

## ■ Agenda - Summary

- Purpose of Water Treatment
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# ■ Proper Water Treatment Program – Overall Outcome



## ■ Water Treatment of Central Air-conditioning Cooling System



# THANK YOU

■ Water Treatment of Central Air-conditioning Cooling System